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APPLICATION NO.	FILING DATE	FIRST NAMED INVENTOR	ATTORNEY DOCKET NO.	CONFIRMATION NO.
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10/681,319

10/09/2003

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EXAMINER

MCNELIS, KATHLEEN A

ART UNIT

PAPER NUMBER

1742

SHORTENED STATUTORY PERIOD OF RESPONSE	MAIL DATE	DELIVERY MODE
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3 MONTHS

01/09/2007

PAPER

Please find below and/or attached an Office communication concerning this application or proceeding.

If NO period for reply is specified above, the maximum statutory period will apply and will expire 6 MONTHS from the mailing date of this communication.

Office Action Summary

Application No.

10/681,319

Applicant(s)

ASANO ET AL.

Examiner

Kathleen A. McNelis

Art Unit

1742

-- The MAILING DATE of this communication appears on the cover sheet with the correspondence address --

Period for Reply

A SHORTENED STATUTORY PERIOD FOR REPLY IS SET TO EXPIRE 3 MONTH(S) OR THIRTY (30) DAYS, WHICHEVER IS LONGER, FROM THE MAILING DATE OF THIS COMMUNICATION.

- Extensions of time may be available under the provisions of 37 CFR 1.136(a). In no event, however, may a reply be timely filed after SIX (6) MONTHS from the mailing date of this communication.
- If NO period for reply is specified above, the maximum statutory period will apply and will expire SIX (6) MONTHS from the mailing date of this communication.
- Failure to reply within the set or extended period for reply will, by statute, cause the application to become ABANDONED (35 U.S.C. § 133). Any reply received by the Office later than three months after the mailing date of this communication, even if timely filed, may reduce any earned patent term adjustment. See 37 CFR 1.704(b).

Status

- 1) ☒ Responsive to communication(s) filed on 02 November 2006.
- 2a) ☐ This action is FINAL. 2b) ☒ This action is non-final.
- 3) ☐ Since this application is in condition for allowance except for formal matters, prosecution as to the merits is closed in accordance with the practice under *Ex parte Quayle*, 1935 C.D. 11, 453 O.G. 213.

Disposition of Claims

- 4) ☒ Claim(s) 1-4,6-12 and 14-19 is/are pending in the application.
- 4a) Of the above claim(s) _____ is/are withdrawn from consideration.
- 5) ☐ Claim(s) _____ is/are allowed.
- 6) ☒ Claim(s) 1-4,6-12 and 14-19 is/are rejected.
- 7) ☐ Claim(s) _____ is/are objected to.
- 8) ☐ Claim(s) _____ are subject to restriction and/or election requirement.

Application Papers

- 9) ☐ The specification is objected to by the Examiner.
- 10) ☐ The drawing(s) filed on _____ is/are: a) ☐ accepted or b) ☐ objected to by the Examiner.
- Applicant may not request that any objection to the drawing(s) be held in abeyance. See 37 CFR 1.85(a).
- Replacement drawing sheet(s) including the correction is required if the drawing(s) is objected to. See 37 CFR 1.121(d).
- 11) ☐ The oath or declaration is objected to by the Examiner. Note the attached Office Action or form PTO-152.

Priority under 35 U.S.C. § 119

- 12) ☒ Acknowledgment is made of a claim for foreign priority under 35 U.S.C. § 119(a)-(d) or (f).
- a) ☐ All b) ☐ Some * c) ☐ None of:
1. ☒ Certified copies of the priority documents have been received.
2. ☐ Certified copies of the priority documents have been received in Application No. _____.
3. ☐ Copies of the certified copies of the priority documents have been received in this National Stage application from the International Bureau (PCT Rule 17.2(a)).
- * See the attached detailed Office action for a list of the certified copies not received.

Attachment(s)

- 1) ☒ Notice of References Cited (PTO-892)
- 2) ☐ Notice of Draftsperson's Patent Drawing Review (PTO-948)
- 3) ☐ Information Disclosure Statement(s) (PTO/SB/08)
Paper No(s)/Mail Date _____
- 4) ☐ Interview Summary (PTO-413)
Paper No(s)/Mail Date. _____
- 5) ☐ Notice of Informal Patent Application
- 6) ☐ Other: _____

Claims Status

Claims 1-4, 6-12 and 14-19 remain for examination where claim 1 is amended.

Acknowledgement of RCE

A request for continued examination under 37 CFR 1.114, including the fee set forth in 37 CFR 1.17(c), was filed in this application after final rejection. Since this application is eligible for continued examination under 37 CFR 1.115, and the fee set forth in 37 CFR 1.17(e) has been timely paid, the finality of the previous office action has been withdrawn pursuant to 37 CFR 1.114. Applicant's submission filed on 11/02/2006 has been entered.

Priority

Receipt is acknowledged of papers submitted under 35 U.S.C. 119(a)-(d), which papers have been placed of record in the file.

Status of Previous Rejections

The following rejections are withdrawn in view of amendments to the claims:

- Claims 1, 3, 4, 7, 9, 11, 12, 15, 17 and 18 under 35 U.S.C. 102(b) as being anticipated by Bruening et al. (U.S. Pat. No. 5,120,443),
- Claims 2, 6, 10 and 14 under 35 U.S.C. 103(a) as being unpatentable over Bruening et al. (U.S. Pat. No. 5,120,443) in view of EP 1,167,555 (EP '555),
- Claims 8 and 16 under 35 U.S.C. 103(a) as being unpatentable over Bruening et al. (U.S. Pat. No. 5,120,443) in view of Ji et al. (U.S. Pat. No. 6,660,059), and
- Claim 19 under 35 U.S.C. 103(a) as being unpatentable over Bruening et al. (U.S. Pat. No. 5,120,443).

Claim Rejections - 35 USC § 103

The text of those sections of Title 35, U.S. Code not included in this action can be found in a prior Office action.

Claims 1, 3, 4, 7, 9, 11, 12, 15, and 17-19 are rejected under 35 U.S.C. 103(a) as being unpatentable over Bruening et al. (U.S. Pat. No. 5,120,443) in view of Japanese Patent 62-238337 (JP '337)¹.

With respect to claims 1 and 19, Bruening et al. discloses a method for removing, separating and concentrating rhodium (Rh), iridium (Ir) and Ruthenium (Ru) from a source containing other ions by bringing the source solution into contact with a polyalkylene-polyamine containing ligand covalently bonded through an organic spacer silicon grouping to a solid inorganic support (abstract). The "other ions" are impurity elements as in instant claim 1. The "polyalkylene-polyamine containing ligand covalently bonded through an organic spacer silicon grouping to a solid inorganic support" is substantially similar to a polyamine based anion exchange resin as in instant claim 1, since the functional group (polyamine) is the same. Bruening et al. discloses the following process in example 9:

- Contacting a polyamine based resin with a source solution containing Rh, Ru, Ir and Cu, drawing the solution through the resin with a vacuum pump (col. 13 lines 24-32), which is equivalent to the first step in instant claim 1.
- Washing the resin with 50 mL of 0.1 M HCl (col. 13 lines 31-33), which is equivalent to the second step in instant claim 1.
- Subsequently recovering Rh and Ru in a recovery solution of thiourea plus HCl by drawing this recovery solution through the resin, thereby recovering greater than 99% of the Rh and Ru from the source solution with no Ir or Cu impurity detected in the solution (col. 13 lines 32-47), which is substantially similar to the third step in instant claim 1, however the exemplary solution of Bruening et al. contains additional substances and is not contacted in successive steps.

¹ Based on English abstract. A translation will be provided by USPTO when available.

Bruening et al. does not recite that the polyamine ligand is a resin, or that the elution step comprises bringing the washing-treated resin into contact with an aqueous solution consisting of water and thiourea or with a first aqueous solution consisting of water and thiourea and then a second aqueous solution consisting of water and hydrochloric acid successively.

JP '337 discloses a method for separating and recovering noble platinum group metals (e.g. Pd, Pt, Rh) from other ions by passing through a primary-quaternary (i.e. poly) amine anion exchange resin, followed by elution in a 0.1N HCl and 0.1M thiourea solution to recover the noble metals at high yield (abstract). It would have been obvious to one of ordinary skill in the art at the time the invention was made to use the primary-quaternary (i.e. poly) amine anion exchange resin and 0.1N HCl and 0.1M thiourea solution of JP '337 in the process of Bruening et al. to recover the noble metals (e.g. Pd, Pt, Rh) at high yield as taught by JP '337.

While Bruening et al. in view of JP '337 does not teach that the contact of the aqueous HCl and thiourea solution are successive (JP '337 recites a mixture of the two solutions), it is the examiner's position that the applicants' have not established the criticality of the sequential contacting step (i.e. thiourea followed by HCl) by showing unexpected results. The selection of any order of performing process steps is prima facie obvious in the absence of any new or unexpected results (MPEP section 2144.04 IV, C).

With respect to instant claim 3, the wash solution is dilute (0.1 M) HCl as discussed above regarding claim 1. With respect to claim 4, the diluted HCl solution has a chloride ion concentration of 0.1 M as discussed above regarding claim 1, which is less than 4 mol/L.

With respect to claim 7, Bruening et al. discloses a process for separating and recovering Ir, Ru, Rh from a solution with impurities as described above regarding claim 1, wherein the receiving solution is a thiourea and hydrochloric solution (example 9) as described above

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regarding claim 1. The temperature of the thiourea solution is disclosed in example 9 as 70 °C (col. 13 lines 24-47), which is within the claimed range of between 60 and 90 °C.

With respect to claims 9, 11, 12 and 15, Bruening et al. teaches that the PGM is at least one element selected from the group of Ir, Rh and Ru (abstract) and JP '337 discloses examples of Pt, Pd and Rh (abstract).

With respect to claims 17 and 18, the elution step comprises bringing the washing-treated resin into contact with a solution containing thiourea and hydrochloric acid.

Claims 2, 6, 10 and 14 are rejected under 35 U.S.C. 103(a) as being unpatentable over Bruening et al. (U.S. Pat. No. 5,120,443) in view of ~~of prior art~~ of Japanese Patent 62-238337 (JP '337) as applied to claim 1 and further in view of EP 1,167,555 (EP '555).

Bruening et al. in view of JP '337 is applied as discussed above regarding claim 1.

Further, Bruening et al. teaches that the process relies on the ability to first selectively attract and bind, then to selectively remove (i.e. elute) complexes of Rh, Ir and Ru (col. 7 lines 27-60).

Bruening et al. does not teach that the chloride solution is maintained at an ORP of 700 to 1100 mV as in claim 2, or that the HCl solution has a chloride ion concentration of 4 mol/L or more as in claim 6.

EP '555 teaches a method of chromatographic interseparation of PGM wherein Rh and Ir are eluted as separate fractions [0001]. EP '555 teaches that in prior art applications, the elution of Ir was slow and the resulting metal concentration dilute compared to other metal fractions [0006]. EP '555 teaches an improvement to the prior art, using a 3-6 M HCl solution [0022] and bringing the redox potential to between 770 and 900 mV to control the oxidative state of Ir. This provides

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the maximum separation of Ir from Rh [0009-0010]. ORP and concentration of eluting solutions are therefore recognized as result-effective variables in the art, which are varied to affect the absorption and elution of metals of interest. It would have been obvious to one of ordinary skill in the art at the time the invention was made to adjust the solution concentration and ORP as result-effective variables to affect the metal absorption and elution from the resin (see M.P.E.P 2144.05, II, B). Further, it would have been obvious to one of ordinary skill in the art at the time the invention was made to vary the ORP and elution steps by using a 3-6 M HCl solution while maintaining a redox potential of between 770 and 900 mV as taught by EP '555 in the PGM separation process of Bruening et al. in view of JP '337 to achieve maximum separation of Ir from Rh as taught by EP '555. The ORP range taught by EP '555 of between 770 and 900 mV is within the claimed range of 700 to 1100 mV. The range of between 3-6 M HCl overlaps with the claimed range of 4 mol/L or more in claim 6. It would have been obvious to one of ordinary skill in the art at the time the invention was made to elute with a HCl solution of between 4 and 6 mol/L since EP '555 teaches that a solution of between 3-6 M HCl is preferred [0022].

With respect to claims 10 and 14, Bruening et al. teaches that the PGM is at least one element selected from the group of Ir, Rh and Ru (abstract) and JP '337 discloses examples of Pt, Pd and Rh (abstract).

Claims 8 and 16 are rejected under 35 U.S.C. 103(a) as being unpatentable over Bruening et al. (U.S. Pat. No. 5,120,443) in view ~~of in view~~ of Japanese Patent 62-238337 (JP '337) as applied to claim 1 and further in view of Ji et al. (U.S. Pat. No. 6,660,059).

Bruening et al. in view of JP '337 is applied as discussed above regarding claim 1.

Bruening et al. in view of JP '337 does not teach that the elution effluent is subsequently made alkaline, then heated to recover the PGM in the form of sulfide as in instant claim 8.

Ji et al. discloses a process for recovering precious metals from refractory materials (abstract), wherein Ji et al. defines precious metals to include PGM (col. 1, lines 20-25). Following separation of the precious metal bearing solution, the pH of the solution is adjusted to alkaline conditions and the precious metals are precipitated as sulfides (col. 13 lines 45-67). The temperature is maintained between about 5 and 40 °C (col. 14 lines 1-16) which range includes a portion that is “heated” as in instant claim 8. Ji et al teaches that recovering the precious metal in this way reduces impurities in the solution (col. 13 lines 45-67) and results in relatively high rates of precious metal recovery (abstract). It would have been obvious to one of ordinary skill in the art at the time the invention was made to precipitate the PGM as a sulfide by increasing the solution pH as taught by Ji et al. following separation in the process of Bruening et al. in view of JP ‘337 to benefit from relatively high rates of precious metal recovery as taught by Ji et al.

Bruening et al. in view of JP ‘337 and Ji et al. does not disclose heating the solution prior to recovery of the PGM, however, it is well settled that where the principal difference between a claimed process and that taught by reference is a temperature difference, it is incumbent upon applicants to establish the criticality of that difference (Ex parte Khusid, et al., 174 USPQ 59).

With respect to claim 16 Bruening et al. discloses that the PGM is at least one element selected from the group of Ir, Rh and Ru (abstract) and JP ‘337 discloses examples of Pt, Pd and Rh (abstract).

Claims 1, 3, 4, 7, 9, 11, 12, 15, and 17-19 are rejected under 35 U.S.C. 103(a) as being unpatentable over Japanese Patent 62-238337 (JP ‘337)¹ in view of Fieberg et al. (U.S. Pat. No. 4,105,443) and Bruening et al. (U.S. Pat. No. 5,120,443)

With respect to claims 1, 3 and 4, JP ‘337 discloses a method for separating and recovering noble platinum group metals (e.g. Pd, Pt, Rh) from other ions by passing through a primary-

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quaternary (i.e. poly) amine anion exchange resin (essentially the first step in instant claim 1), followed by elution in a 0.1N HCl and 0.1M thiourea solution (essentially the third step in instant claim 1) to recover the noble metals at high yield (abstract).

While JP '337 does not teach that the contact of the aqueous HCl and thiourea solution are successive (JP '337 recites a mixture of the two solutions), it is the examiner's position that the applicants' have not established the criticality of the sequential contacting step (i.e. thiourea followed by HCl) by showing unexpected results. The selection of any order of performing process steps is prima facie obvious in the absence of any new or unexpected results (MPEP section 2144.04 IV, C).

JP '337 does not teach a second step of washing the adsorption-treated resin to form washing-treated resin (step 2 of instant claim 1).

Fieberg et al. discloses a process for separation of ruthenium (abstract) onto quaternary and tertiary (i.e. poly) amine resins (col. 5 lines 52-62). Fieberg et al. teaches washing the loaded resin(s) to remove impurities (col. 5 lines 20-25 and lines 64-65).

Bruening et al. discloses a method for removing, separating and concentrating rhodium (Rh), iridium (Ir) and Ruthenium (Ru) from a source containing other ions by bringing the source solution into contact with a polyalkylene-polyamine containing ligand covalently bonded through and organic spacer silicon grouping to a solid inorganic support (abstract). The "polyalkylene-polyamine containing ligand covalently bonded through an organic spacer silicon grouping to a solid inorganic support" is substantially similar to a polyamine based anion exchange resin in JP '337, since the functional group (polyamine) is the same. Bruening et al. discloses washing the resin with 50 mL of 0.1 M HCl (col. 13 lines 31-33). It would have been obvious to one of ordinary skill in the art at the time the invention was made to wash with dilute HCl solution as

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taught by Bruening et al. the loaded resin of JP '337 to remove entrained impurities as taught by Fieberg et al.

With respect to claim 4, the diluted HCl solution has a chloride ion concentration of 0.1 M as discussed above regarding claim 1, which is less than 4 mol/L.

With respect to claim 7, Bruening et al. discloses a process for separating and recovering Ir, Ru, Rh from a solution with impurities as described above regarding claim 1, wherein the receiving solution is a thiourea and hydrochloric solution (example 9) as described above regarding claim 1. The temperature of the thiourea solution is disclosed in example 9 as 70 °C (col. 13 lines 24-47), which is within the claimed range of between 60 and 90 °C.

With respect to claims 9, 11, 12 and 15, JP '337 discloses examples of Pt, Pd and Rh (abstract) and Bruening et al. teaches that the PGM is at least one element selected from the group of Ir, Rh and Ru (abstract).

Claims 2, 6, 10 and 14 are rejected under 35 U.S.C. 103(a) as being unpatentable over Japanese Patent 62-238337 (JP '337) in view of Fieberg et al. (U.S. Pat. No. 4,105,443) and Bruening et al. (U.S. Pat. No. 5,120,443) as applied to claim 1, and further in view of EP 1,167,555 (EP '555).

JP '337 in view of Fieberg et al. and Bruening et al. is applied as discussed above regarding claim 1.

Further, Bruening et al. teaches that the process relies on the ability to first selectively attract and bind, then to selectively remove (i.e. elute) complexes of Rh, Ir and Ru (col. 7 lines 27-60).

JP '337 in view of Fieberg et al. and Bruening et al. does not teach that the chloride solution is maintained at an ORP of 700 to 1100 mV as in claim 2, or that the HCl solution has a chloride ion concentration of 4 mol/L or more as in claim 6.

EP '555 teaches a method of chromatographic interseparation of PGM wherein Rh and Ir are eluted as separate fractions [0001]. EP '555 teaches that in prior art applications, the elution of Ir was slow and the resulting metal concentration dilute compared to other metal fractions [0006]. EP '555 teaches an improvement to the prior art, using a 3-6 M HCl solution [0022] and bringing the redox potential to between 770 and 900 mV to control the oxidative state of Ir. This provides the maximum separation of Ir from Rh [0009-0010]. ORP and concentration of eluting solutions are therefore recognized as result-effective variables in the art, which are varied to affect the absorption and elution of metals of interest. It would have been obvious to one of ordinary skill in the art at the time the invention was made to adjust the solution concentration and ORP as result-effective variables to affect the metal absorption and elution from the resin (see M.P.E.P 2144.05, II, B). Further, it would have been obvious to one of ordinary skill in the art at the time the invention was made to vary the ORP and elution steps by using a 3-6 M HCl solution while maintaining a redox potential of between 770 and 900 mV as taught by EP '555 in the PGM separation process of JP '337 in view of Fieberg et al. and Bruening et al. to achieve maximum separation of Ir from Rh as taught by EP '555. The ORP range taught by EP '555 of between 770 and 900 mV is within the claimed range of 700 to 1100 mV. The range of between 3-6 M HCl overlaps with the claimed range of 4 mol/L or more in claim 6. It would have been obvious to one of ordinary skill in the art at the time the invention was made to elute with a HCl solution of between 4 and 6 mol/L since EP '555 teaches that a solution of between 3-6 M HCl is preferred [0022].

With respect to claims 10 and 14, JP '337 discloses examples of Pt, Pd and Rh (abstract), and Bruening et al. teaches that the PGM is at least one element selected from the group of Ir, Rh and Ru (abstract).

Claims 8 and 16 are rejected under 35 U.S.C. 103(a) as being unpatentable over Japanese Patent 62-238337 (JP '337) in view of Fieberg et al. (U.S. Pat. No. 4,105,443) and Bruening et al. (U.S. Pat. No. 5,120,443) as applied to claim 1, and further in view of Ji et al. (U.S. Pat. No. 6,660,059).

JP '337 in view of Fieberg et al., Bruening et al. is applied as discussed above regarding claim 1.

JP '337 in view of Fieberg et al., Bruening et al. does not teach that the elution effluent is subsequently made alkaline, then heated to recover the PGM in the form of sulfide as in instant claim 8.

Ji et al. discloses a process for recovering precious metals from refractory materials (abstract), wherein Ji et al. defines precious metals to include PGM (col. 1, lines 20-25). Following separation of the precious metal bearing solution, the pH of the solution is adjusted to alkaline conditions and the precious metals are precipitated as sulfides (col. 13 lines 45-67). The temperature is maintained between about 5 and 40 °C (col. 14 lines 1-16) which range includes a portion that is "heated" as in instant claim 8. Ji et al teaches that recovering the precious metal in this way reduces impurities in the solution (col. 13 lines 45-67) and results in relatively high rates of precious metal recovery (abstract). It would have been obvious to one of ordinary skill in the art at the time the invention was made to precipitate the PGM as a sulfide by increasing the solution pH as taught by Ji et al. following separation in the process of JP '337 in view of Fieberg

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et al., Bruening et al. to benefit from relatively high rates of precious metal recovery as taught by Ji et al.

JP '337 in view of Fieberg et al., Bruening et al. and Ji et al. does not disclose heating the solution prior to recovery of the PGM, however, it is well settled that where the principal difference between a claimed process and that taught by reference is a temperature difference, it is incumbent upon applicants to establish the criticality of that difference (*Ex parte Khusid*, et al., 174 USPQ 59).

With respect to claim 16 JP '337 discloses examples of Pt, Pd and Rh (abstract) and Bruening et al. discloses that the PGM is at least one element selected from the group of Ir, Rh and Ru (abstract).

Response to Arguments

Applicant's arguments with respect to claims 1-4, 6-12 and 14-19 have been considered but are moot in view of the new ground(s) of rejection.

Conclusion

Any inquiry concerning this communication or earlier communications from the examiner should be directed to Kathleen A. McNelis whose telephone number is 571 272 3554. The examiner can normally be reached on M-F 8:00 AM to 4:30 PM.

If attempts to reach the examiner by telephone are unsuccessful, the examiner's supervisor, Roy King can be reached on 571-272-1244. The fax phone number for the organization where this application or proceeding is assigned is 571-273-8300.

Information regarding the status of an application may be obtained from the Patent Application Information Retrieval (PAIR) system. Status information for published applications may be obtained from either Private PAIR or Public PAIR. Status information for unpublished

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applications is available through Private PAIR only. For more information about the PAIR system, see <http://pair-direct.uspto.gov>. Should you have questions on access to the Private PAIR system, contact the Electronic Business Center (EBC) at 866-217-9197 (toll-free). If you would like assistance from a USPTO Customer Service Representative or access to the automated information system, call 800-786-9199 (IN USA OR CANADA) or 571-272-1000.

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